## Solutions to the examination problems on Microfluidics course, 2007

**1.** To solve the problem we will follow a path from the point A to the point B and check the pressure changes:

$$p_A - \gamma_{water} \times 0.2m + \gamma_{oil} * h + \gamma_{water} \times 0.3m = p_B$$

The answer:

$$h = \frac{p_B - p_A + \gamma_{water} \times 0.2m - \gamma_{water} \times 0.3m}{\gamma_{oil}} = 0.449 m$$

2. As 
$$\frac{\partial \vec{V}}{\partial t} = 0$$
, the local acceleration is zero.

From the information on the velocity we can calculate the coefficients a and b:

a=15, b=10.

The velocity is:

$$V = 15 \cdot x + 10 \, m/s$$

and the convective acceleration is:

$$a = 225 \cdot x + 150 \, m / \, s^2$$

at the point x=0, the acceleration  $a=150 m/s^2$ , at the point x=1, the acceleration  $a=375 m/s^2$ .

**3.** To solve the problem we can use control volume approach. Than: along x-axis:

$$V_1 \rho (-V_1) A_1 + V_2 \cos(20^\circ) \rho V_2 A_2 = R_x + p_1 A_1 - p_2 A_2 \cos(20^\circ)$$

Along y-axis:

$$V_1 \rho \left( -V_2 \sin 20^\circ \right) V_2 \rho A_2 = R_v + p_2 A_2 \sin(20^\circ)$$

From the known volume rate, the linear rate can be found (dividing the volume rate by the area). We find that:

$$V_1=3.18 \text{ m/s}; V_2=12.7 \text{ m/s};$$

Missing pressure at the point (2) can be found from Bernoulli equation:

$$P_2 = 74.5 \text{ kPa}$$

And now we have all the data to find the anchoring force:

 $R_x = -822 \text{ N}$ 

$$R_{v} = -156 \text{ N}$$

**4.** Dividing the volumetric rate by the tube area we find the average linear velocity  $\mathbf{V}$  in the tube.  $\mathbf{V}=1.06\text{e-}3 \text{ m/s}$ .

Now the Reynolds number can be found: **Re=1.06**.

As Re<2000 we can conclude that the flow is indeed a **laminar** one.

In the case of laminar flow you expect a parabolic profile for the velocity (MYO, p.328-329):

$$v_z = \frac{1}{4\mu} \left( \frac{\partial p}{\partial z} \right) \left( r^2 - R^2 \right)$$

The velocity in the middle is twice as high as the average velocity V.

(a) the pressure:

$$\Delta p = \frac{8\mu lV}{R^2} = 17 \,\mathrm{Pa}$$

(b) Assuming no mixing, all the liquid A will be situated within a circle of a radius  $R_A$ , which can be found as:

$$\frac{1}{4\mu} \left( \frac{\partial p}{\partial z} \right) \left( R_A^2 - R^2 \right) = \frac{l}{250 \, s}$$

The ratio of the areas containing A and the complete cross-section of the tube will give the percentage reading:

$$\frac{R_A^2}{R^2} = 1 - \frac{4\mu l}{250 \cdot \left| \frac{\partial p}{\partial z} \right|} = 0.058$$

If liquids are inviscid they will move as a plug and A will arrive at the end of the tube after 1/V=0.5/1.06e-3=471 s. After that moment the concentration of A will be 100%.

**5**. As requested in the problem we consider:

$$c = f(\rho, \lambda, h, \sigma)$$

According to the Pi-theorem we should have 5-3=2 Pi-terms. If we use h,  $\rho$ ,  $\sigma$  as repeating variables we get:

$$\Pi_1 = ch^{1/2}\rho^{1/2}\sigma^{-1/2}$$

$$\Pi_1 = \lambda h^{-1}$$

The answer:

$$ch^{1/2}\rho^{1/2}\sigma^{-1/2}=\phi\left(\frac{\lambda}{h}\right)$$